

Modelling of water quality in sewer- WWTP systems during normal and extreme conditions

Period : Oct 2010 – Sep 2013

PhD student: Elham Ramin

Supervisor: Benedek Gy. Plósz (DTU Miljø)

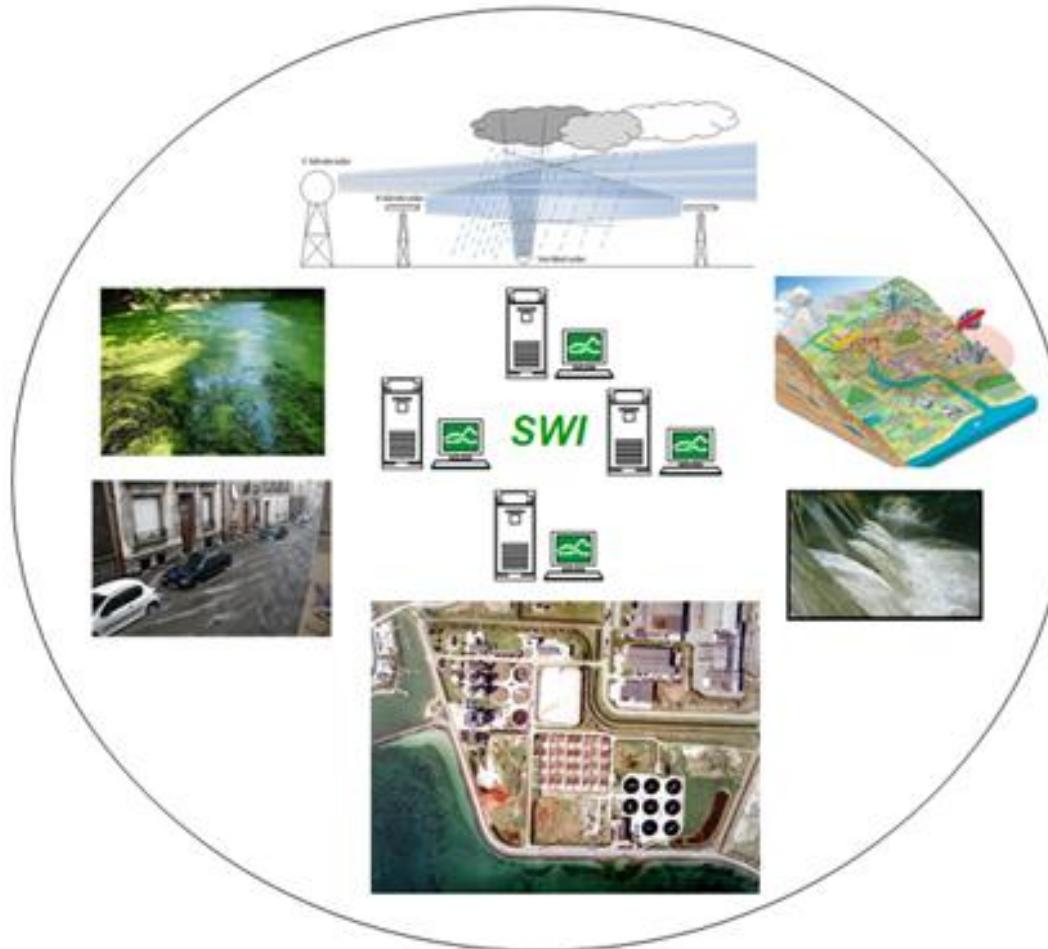
Co-supervisors: Peter Steen Mikkelsen (DTU Miljø)

Michael R. Rasmussen (Aalborg University)

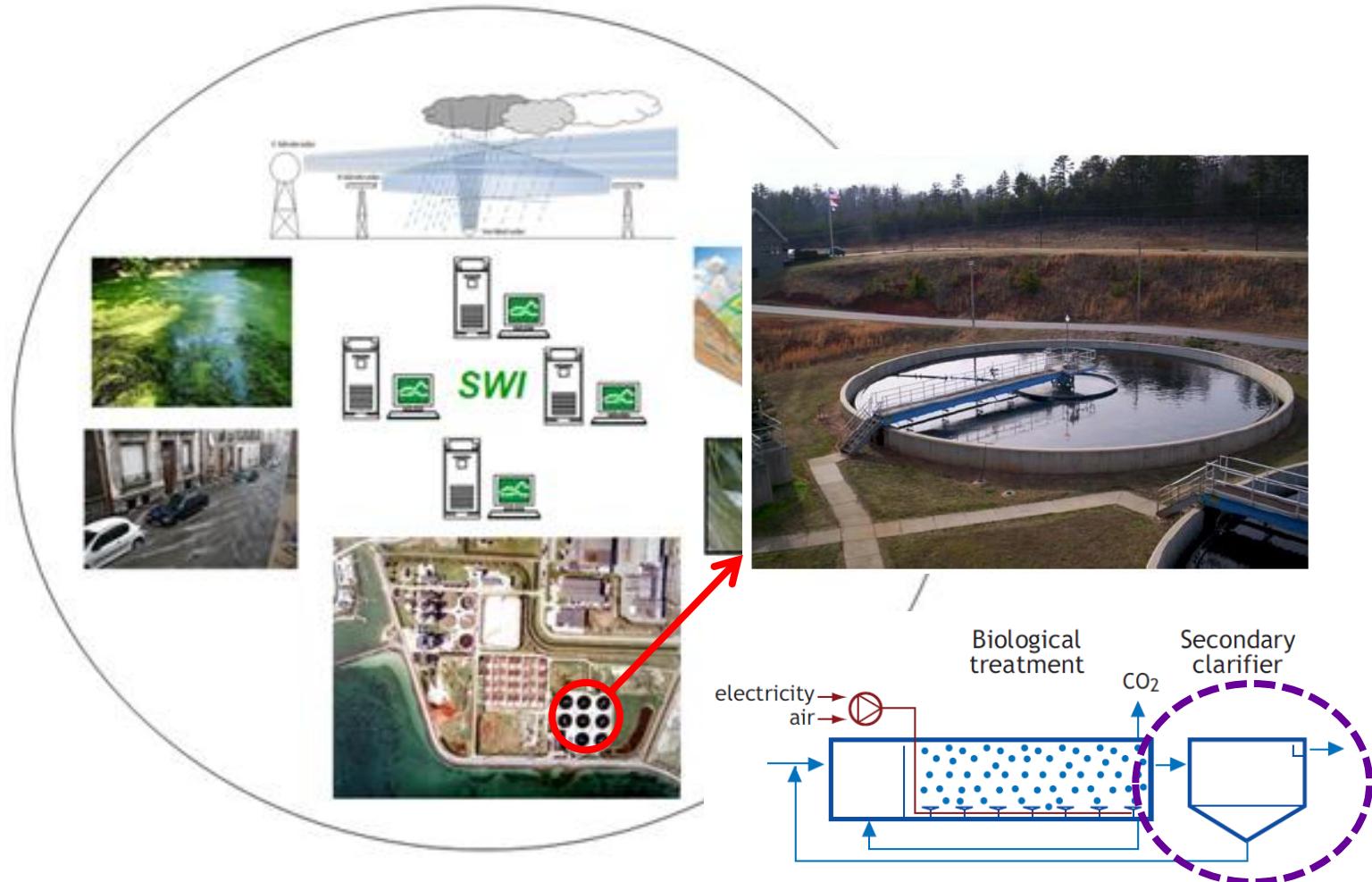
Lars Yde (DHI)

$$\text{CH}_2\text{O} + \text{O}_2 \rightleftharpoons \text{CO}_2 + \text{H}_2\text{O}$$
$$\int_a^b \mathcal{E} \Theta \delta e^{i\pi} = \sqrt{17} \int \Omega \delta e^{i\pi}$$
$$\Delta \sum_{\infty}^{\Sigma} \chi^2 = \{2.718281828459045\}$$

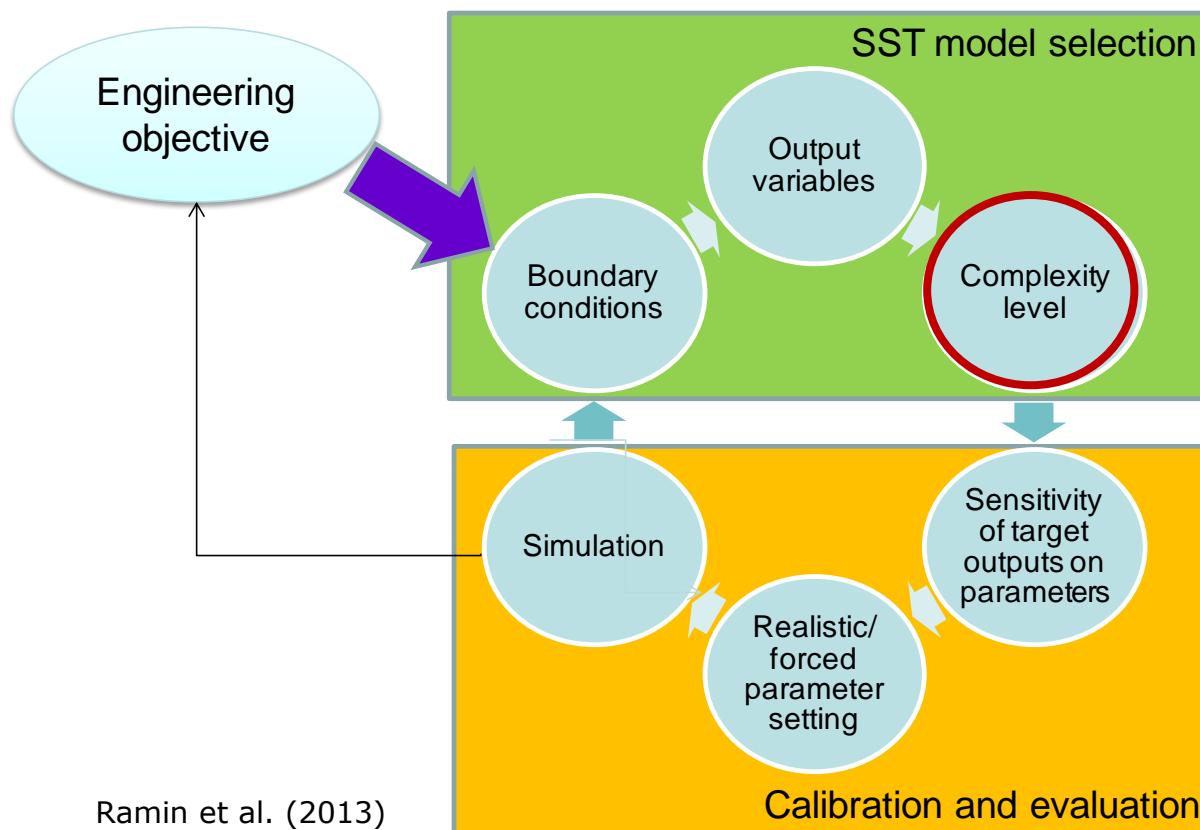
Introduction



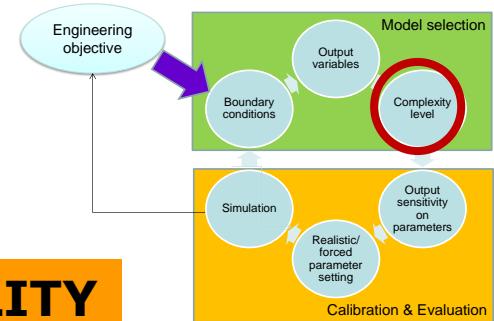
Introduction



Modelling of Secondary Settling Tanks



Complexity level



PROCESS

Advection

Gravity settling

Compression settling

Lumped dispersion

Flocculation

Molecular viscosity

Turbulent viscosity

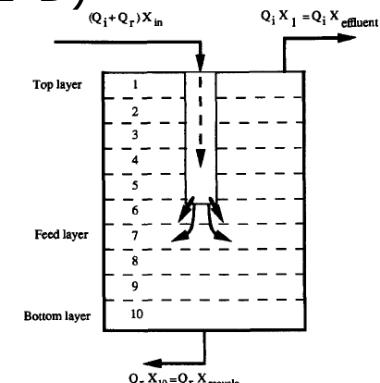
Turbulence

Density

Velocity gradient

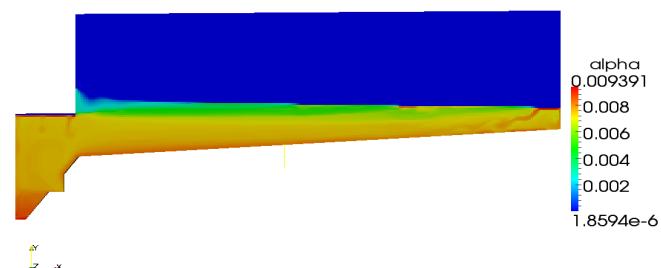
DIMENSIONALITY

- One dimensional (1-D)



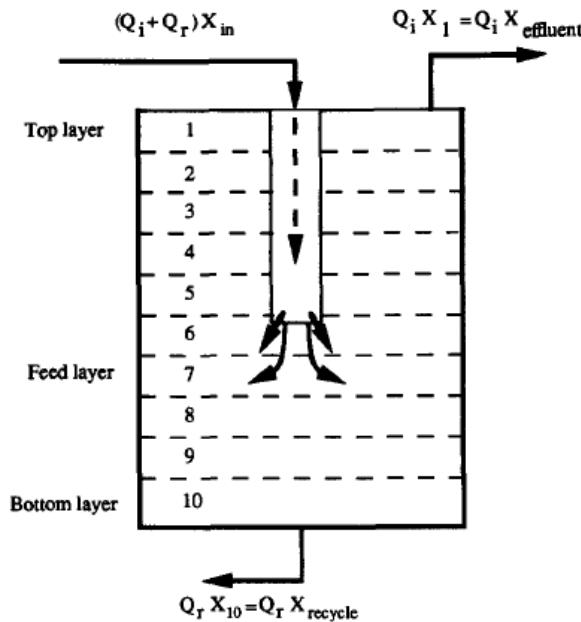
Takács et al. (1991)

- Two- and three-dimensional models:
Computational Fluid Mechanics (CFD)



1-D Secondary settling tank models

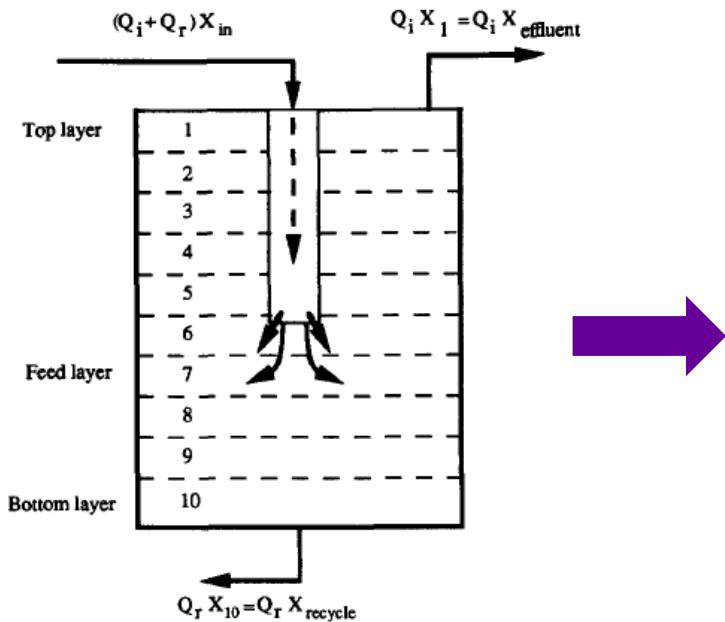
$$-\frac{\partial X_{TSS}}{\partial t} = U \frac{\partial X_{TSS}}{\partial z} - \frac{\partial(v_s X_{TSS})}{\partial z}$$



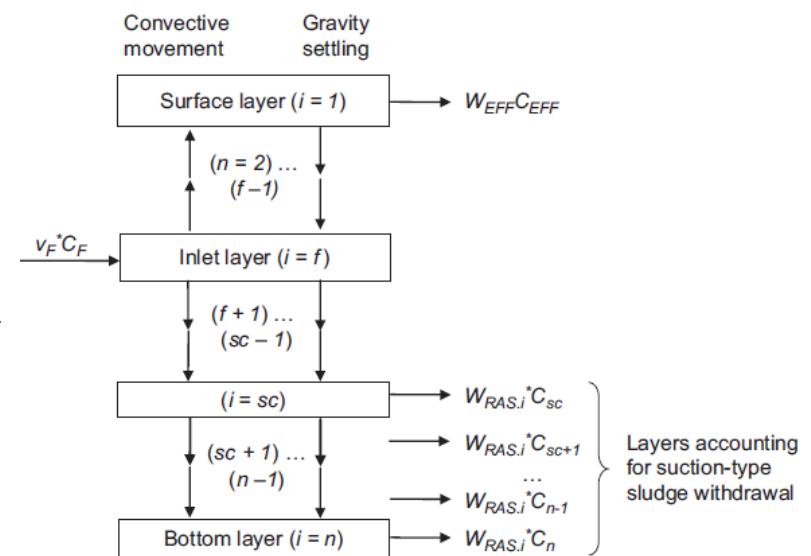
Takács et al. (1991)

1-D Secondary settling tank (SST) models

$$-\frac{\partial X_{TSS}}{\partial t} = U \frac{\partial X_{TSS}}{\partial z} - \frac{\partial(v_s X_{TSS})}{\partial z} \boxed{- D_c \frac{\partial^2 X_{TSS}}{\partial z^2}}$$



Takács et al. (1991)



Plósz et al., 2007

1-D Secondary settling tank (SST) models

$$-\frac{\partial X_{TSS}}{\partial t} = U \frac{\partial X_{TSS}}{\partial z} - \frac{\partial(v_s X_{TSS})}{\partial z} \boxed{- D_c \frac{\partial^2 X_{TSS}}{\partial z^2}}$$

$$v_s = v_0 \left(e^{-r_H(X - f_{NS} \cdot X_F)} - e^{-r_p(X - f_{NS} X_F)} \right)$$

1-D Secondary settling tank model parameters

$$-\frac{\partial X_{TSS}}{\partial t} = U \frac{\partial X_{TSS}}{\partial z} + \frac{\partial(v_s X_{TSS})}{\partial z} - D_c \frac{\partial^2 X_{TSS}}{\partial z^2}$$

$$v_s = v_0 \left(e^{-r_H(X - f_{NS} \cdot X_F)} - e^{-r_p(X - f_{NS} \cdot X_F)} \right)$$

Measurable parameters:
(Settling Characteristics)



1-D Secondary settling tank model parameters

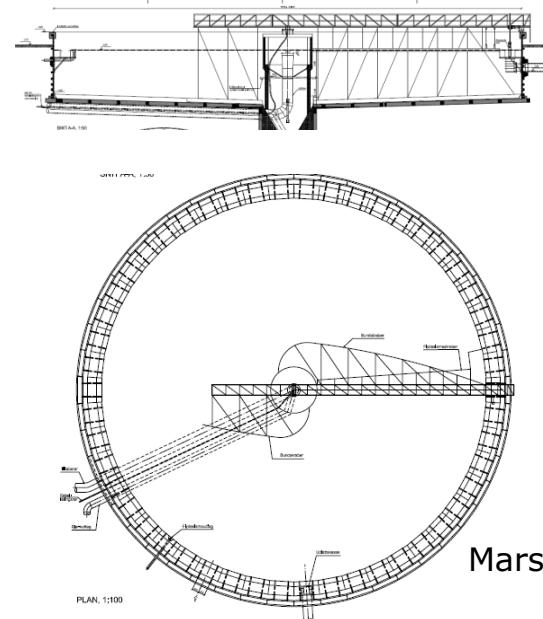
$$-\frac{\partial X_{TSS}}{\partial t} = U \frac{\partial X_{TSS}}{\partial z} + \frac{\partial(v_s X_{TSS})}{\partial z} - D_C \frac{\partial^2 X_{TSS}}{\partial z^2}$$

$$v_s = v_0 \left(e^{-r_H(X - f_{NS} \cdot X_F)} - e^{-r_p(X - f_{NS} \cdot X_F)} \right)$$

Measurable parameters:
(Settling Characteristics)



Calibrated parameter:
(Design&flow Characteristics)



Phase I. Global sensitivity Analysis

Objective

Show the **significance** of explicit **model parameters and dynamic behavior** of **1-D secondary settler models** on the biokinetic model **prediction in WWTP models**

Relative importance of secondary settling tank models in WWTP simulations – A global sensitivity analysis using BSM2

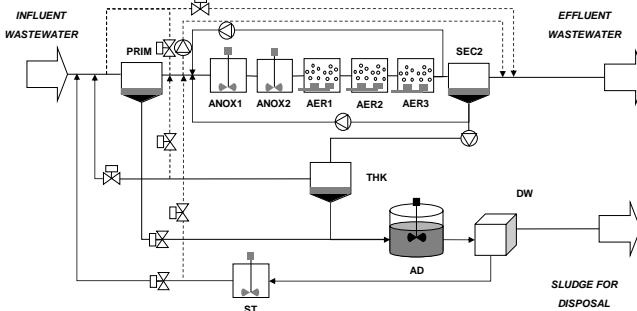
Elham Ramin, Xavier Flores-Alsina, Gürkan Sin, Krist V. Gernaey, Ulf Jeppsson,
Peter Steen Mikkelsen, Benedek Gy. Plósz*

Parameters

μ_{H^-} = [3; 5]
 K_S = [5 ;15]
 K_{OH^-} = [0.1; 0.3]
 $K_{NO_3^-}$ = [0.25; 0.75]
 b_H^- = [0.29 ;0.32]
 μ_A^- = [0.48 ;0.53]
 $K_{NH_4^+}$ = [0.50 ;1.50]
 K_{OA^-} = [0.3 ;0.5]
.
.
.
DSVI = [50 ;200]
 r_P = [2.7e-3;10e-3]
 f_{ns} = [1.23e-3 ;2.59e-3]
 $V_{F,CON}$ = [25; 40]
 $V_{OV,DIS}$ = [10; 22]

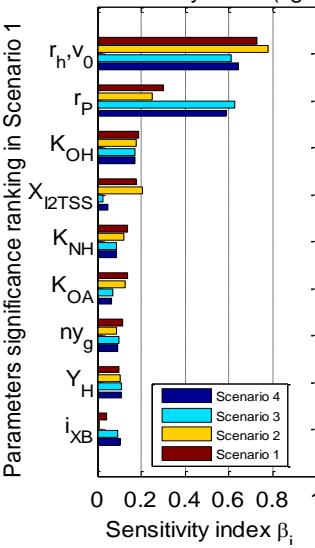


Monte Carlo Simulation

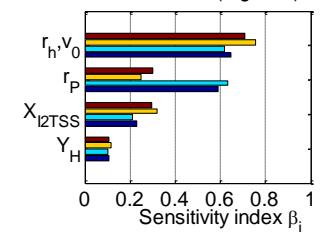


Sensitivity rankings

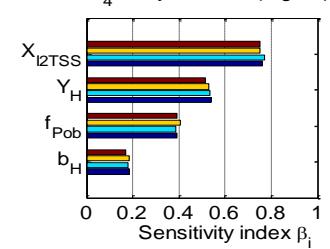
Effluent Quality Index (kg/day)



Effluent TSS (mg SS/l)



NH_4 in reject water (mg N/l)



Phase II. Fluid dynamics in secondary settling tanks (CFD simulations)

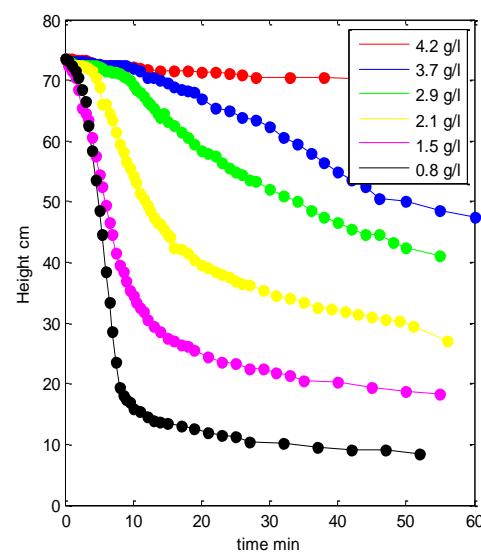
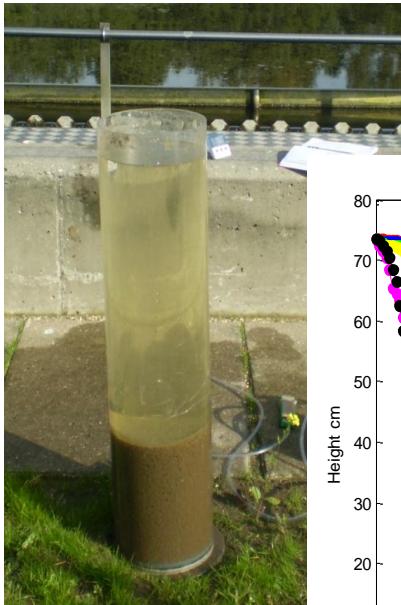
Objective

To generate **numerical experimental data** sets using transient-to-steady-state (and, if possible, dynamic) CFD simulations for secondary settling tanks with **different design and flow boundary conditions**. We then use the obtained data sets to **optimize and calibrate 1-D secondary settling tank models**.

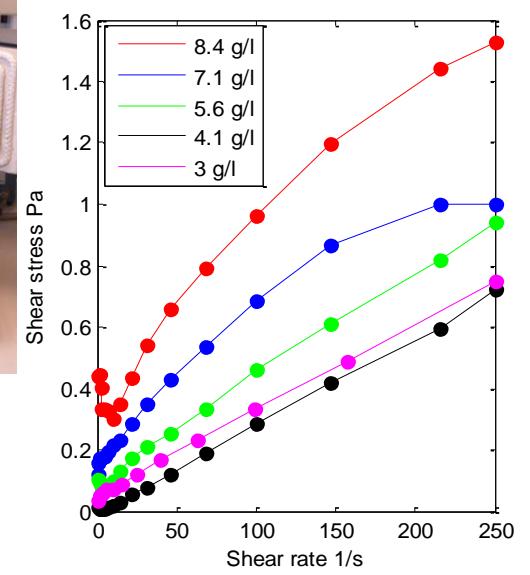
Phase II. CFD simulations

1. Sub-model optimization and calibration

Settling test



Rheology test



Phase II. CFD simulations

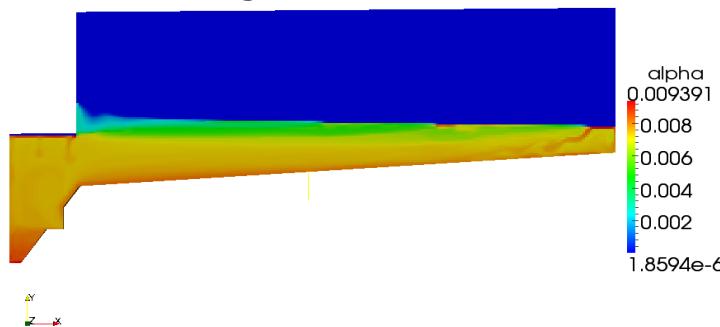


2. CFD simulation of the settling tank

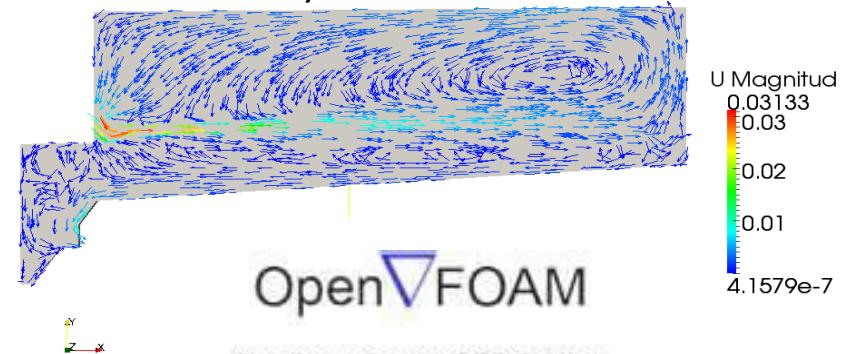
Lundtofte WWTP, Clarifier number 3



Sludge distribution



Velocity field

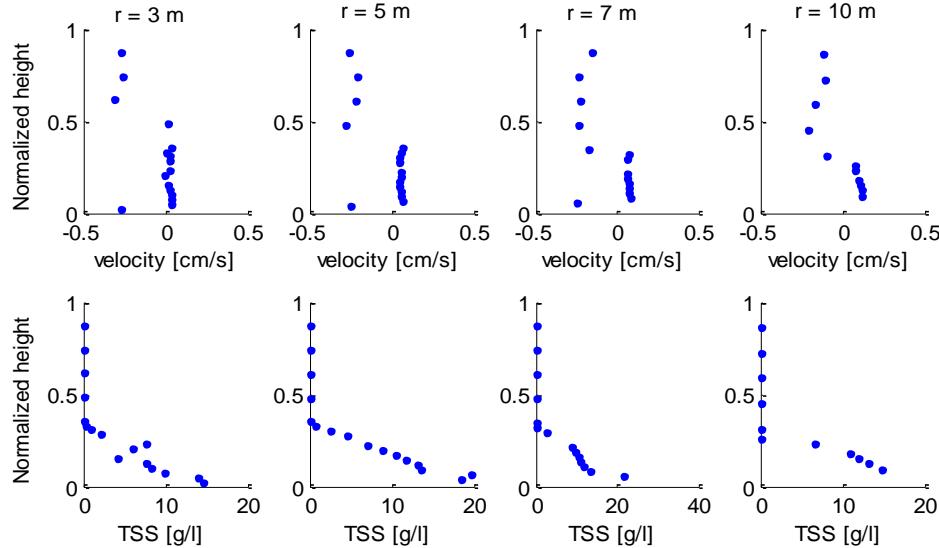


Phase II. CFD simulations

Lundtofte WWTP, Clarifier number 3

3. Model evaluation

Measurement campaign on a full-scale secondary settling tank

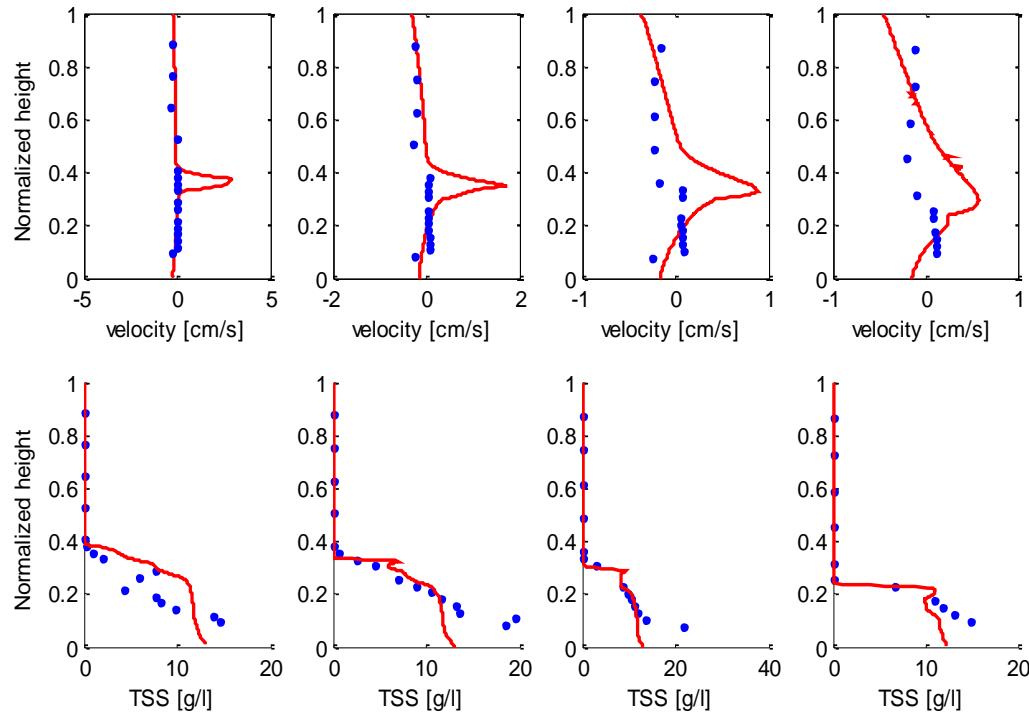


TSS and velocity sensors used for profile measurements

Phase II. CFD simulations



Measured vs. simulated profiles



CFD —————
measured ●

Phase II. CFD simulations

4. Creating an inventory of CFD simulations

In terms of design and flow boundary conditions



Phase III. optimize and calibrate 1-D secondary settling tank models

Objective

A more **mechanistic** way for hydrodynamics modeling in 1-D that could account for **different design and flow** boundary conditions

1-D model optimization

Approach I: calibrate dispersion, downward convection and dynamic-feed layer position models to account for different clarifier design.

Approach II: Testing theories that could unify 1-D hydrodynamic model calibrations obtained for different SST structure



Thank you!



Spildevandscenter Avedøre



aarhusvand



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KRÜGER



Lynettefællesskabet I/S